

# **Test Report**

BD Medical 920 East 19<sup>th</sup> Street Columbus, Nebraska 68601

EO Sterilization Chamber EO DRE Test

Test Date: July 12, 2019

AST Project No. 2019-0436D

Prepared By
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# **Regulatory Information**

Permit No.(s) Regulatory Citation(s)

40 CFR Part 63, Subpart O

# **Source Information**

Source Name
Sterilization Chamber –
Catalytic Oxidizer

Target Parameter(s)
Ethylene Oxide - DRE

# **Contact Information**

Test Location
BD Medical
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Columbus, Nebraska 68601

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Alliance Source Testing, LLC (AST) has completed the source testing as described in this report. Results apply only to the source tested and operating conditions for the specific test date and time(s) identified within this report. All results are intended to be considered in their entirety, and AST is not responsible for use of less than the complete test report without written consent. This report shall not be reproduced in full or in part without written approval from the customer.

To the best of my knowledge and abilities, all information, facts and test data are correct. Data presented in this report have been checked for completeness and are accurate, error-free and legible. Onsite testing was conducted in accordance with approved procedures. Any deviations or problems are detailed in the relevant sections on the test report.

This report is only considered valid once an authorized representative of AST has signed in the space provided below; any other version is considered draft. This document was prepared in portable document format (.pdf) and contains pages as identified in the bottom footer of this document.

Marty Willinger, QI Report Writer

Alliance Source Testing, LLC

July 26, 2018

Date

July 26, 2018

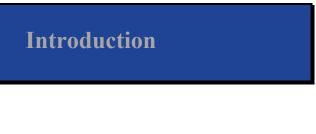
Date

Kenneth Moody Field Team Leader Alliance Source Testing, LLC



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## 1.0 Introduction

Alliance Source Testing, LLC (AST) was retained by Becton-Dickinson Medical (BD Medical) to conduct compliance testing on the ethylene oxide (EO) sterilization chamber at the BD Medical facility located in Columbus, Nebraska. A performance test was conducted to quantify the concentrations and mass rates of EO into and out of the catalytic oxidizer to determine the EO destruction removal efficiency (DRE) on a mass basis. The performance test was conducted to satisfy testing requirements and demonstrate compliance with emission standards outlined in 40 CFR Part 63, Subpart O – Ethylene Oxide Emissions Standards for Sterilization Facilities. The catalytic oxidizer is required to demonstrate 99% DRE of EO.

## 1.1 Facility Description/ Source and Control System Descriptions

An EO sterilization chamber is in service at the BD Medical facility in Columbus, Nebraska. A catalytic oxidizer is used for control of EO emissions. The source identification and operating standards are provided in Table 1-1.

Table 1-1
Emission Limits

Source	Pollutant	Citation
Catalytic Oxidizer	Ethylene Oxide DRE $\geq$ 99% Catalyst bed outlet temperature to be recorded	40 CFR Part 63, Subpart O

## 1.2 Test Protocol & Notification

Testing was conducted in accordance with the test protocol submitted to NDEQ by BD Medical.

## 1.3 Test Program Notes

No test method deviations occurred during testing, expect as noted in the test protocol.

At the inlet sampling location, AST did not conduct EPA Method 4 sampling for measuring moisture content, due to possible EO exposure risks. Moisture content was measured from the outlet sampling location and used for both the inlet and outlet volumetric flow calculations and converting EO concentrations to a dry basis. EPA Method 4 sampling was completed from a single sample point at the outlet sampling location.

**Summary of Results** 



# 2.0 Summary of Results

AST conducted compliance testing on the EO sterilization chamber on July 12, 2019.

Three (3), 1-hour test runs will be conducted to determine the concentrations of EO into and out of the sterilization chamber. Concurrent volumetric flow rate (VFR) measurements were conducted to calculate mass rates. Since the contents of the gas streams are is essentially air, a dry molecular weight of 29.0 was assumed for gas velocity calculations. EO DRE was determined by comparing the inlet and outlet EO levels on a mass basis.

To determine the inlet and outlet levels of EO, direct-interface EPA Method 18 on-site gas chromatographs equipped with flame ionization detectors (GCFID). The GCFID were calibrated with EO balanced nitrogen standards certified to 2% accuracy and dilutions of certified standards.

The involved processes were operating under normal conditions. Applicable operating and control equipment parameters were recorded throughout the test program by BD Medical personnel for inclusion in the test report, including;

# • Catalyst bed outlet temperature

Table 2-1 provide a summary of the emission testing results with comparisons to the applicable limits. Any difference between the summary results listed in the following table and the detailed results contained in appendices are due to rounding for presentation.

Table 2-1
Summary of Results

Emissions Data							
Run Number	1	2	3	Average	Emission		
Date	07/12	07/12	07/12		Standard		
Operating Data							
Catalyst Bed Outlet Temperature, °C	165	185	189	180			
Inlet Data							
H <sub>2</sub> O Concentration, %vd	3.5	3.5	2.7	3.1			
VFR, dscfm	4,022	4,008	3,772	3,934			
EO Concentration, ppmvd	854.0	1105.7	1366.3	1108.7			
EO Rate, lb/hr	23.56	30.39	35.34	29.76			
Outlet Data							
H <sub>2</sub> O Concentration, %vd	3.5	3.5	2.7	3.1			
VFR, dscfm	3,959	3,768	3,803	3,844			
EO Concentration, ppmvd	0.11	0.11	0.12	0.12			
EO Rate, lb/hr	0.0031	0.0029	0.0032	0.0031			
DRE Data							
EO DRE (lb/hr), %	99.99	99.99	99.99	99.99	≥ 99		

**Testing Methodology** 



# 3.0 Testing Methodology

Testing was conducted in accordance with U.S. Environmental Protection Agency (EPA) Reference Test Methods (RM) 1, 2, 4 and 18 referenced in 40 CFR Part 60, Appendix A. The emission testing program was conducted in accordance with the test methods listed in Table 3-1. Method descriptions are provided below while quality assurance/quality control (QA/QC) data are provided in Appendix C.

Table 3-1
Source Testing Methodology

Parameter	U.S. EPA Reference Test Methods	Notes
VFR	1-2	Full Velocity Traverses
$O_{2}$ , $CO_{2}$	2	Assumed Ambient
H <sub>2</sub> O	4	Gravimetric Analysis
EO	18	Gas Chromatograph

#### 3.1 U.S. EPA Reference Test Methods 1 and 2 – Volumetric Flow Rate

The sampling location and number of traverse points were selected in accordance with EPA RM 1. To determine the minimum number of traverse points, the upstream and downstream distances were equated into equivalent diameters and compared to Figure 1-2 in EPA RM 1. All stack diameters, depths, widths, upstream and downstream disturbance distances and nipple lengths were measured on site with a verification measurement provided by the Field Team Leader.

Full velocity traverses were conducted in accordance with EPA RM 2 to determine the stack gas velocity pressure, static pressure and temperature. The velocity and static pressure measurement system consisted of a pitot tube and inclined manometer. The stack gas temperature was measured with a K-type thermocouple and pyrometer. The pitot assembly was leak checked pre and post each sampling period.

The temperature and differential pressure traverse data were combined with concurrently collected diluent data to calculate the stack gas velocity and volumetric flow rate in units of feet per second (ft/sec), actual cubic feet per minute (acfm), dry standard (1 atmosphere and 68°F) cubic feet per minute (dscfm) and pounds per hour (lb/hr). Since the contents of the gas streams are is essentially air, a dry molecular weight of 29.0 was assumed for gas velocity calculations.

## 3.2 U.S. EPA Reference Test Method 4 – Moisture Content

The stack gas moisture content was determined in accordance with EPA RM 4.

For each test run, a sample of gas for moisture determination was extracted from the stack at a constant flow rate of no more than 0.75 cubic feet per minute (cfm). The gas sample was passed through a stainless-steel probe, through a series of four (4) chilled glass impingers, and through a calibrated dry gas meter. In lieu of EPA RM 4 Section 8.1.1.1 requirements, a single sample point was used for moisture determination.

Prior to sampling, the first two impingers each were seeded with 100 milliliters of water. The third impinger was empty. The fourth impinger was seeded with 250 grams of dried silica gel. The sampling system was leak checked



pre and post each sampling period. Following sampling, the moisture gain in the impingers was measured gravimetrically and compared to the total sample volume (standard conditions) to determine the moisture content of the gas. The measured moisture content was compared to the saturation moisture content at stack temperature and pressure. The lower of the two moisture content values was reported.

# 3.3 U.S. EPA Reference Test Method 18 – Ethylene Oxide

Ethylene oxide concentrations were measured in accordance with EPA RM 18 using the direct interface sampling and analysis procedures detailed in the method. Samples were analyzed on-site with an HP Model 5890 Series II Gas Chromatograph equipped with dual RTX-1 columns to separate methane and EO, dual flame ionization detectors (FID) and Chemstation software.

Gas phase calibration standards were prepared by dilution of  $\pm -2\%$  accuracy certified gas standards. Preparation of diluted standards were conducted using a gas-tight volumetric syringe and new Tedlar bags. Triplicate injections were conducted for each standard, and a calibration curve of peak area versus concentration was prepared. A least squares line (y=mx) was fit to the inlet and outlet data set.

Following the GC calibrations, a recovery study (line loss) was conducted using certified EO gas standards with approximate concentrations of approximately 5,000 ppm and 50 ppm of EO for the inlet and outlet sampling systems, respectively. A successful recovery study was demonstrated with the mean, triplicate GC response within 10% of the certified gas concentration.

EO levels were measured at the inlet and outlet simultaneously. A gas sample was transported directly to the GC gas sampling valves using a heated sample line. Samples were analyzed approximately once every 10-minutes. A "test run" consisted of five (5) consecutive injections. Three (3), test runs were conducted (for a total of 15 injections) at the inlet and outlet of the catalytic oxidizer.

After completing the 3 test runs, the mid-level calibration standards were re-analyzed at the gas sampling valve in triplicate. The average of the initial calibration response (triplicate average) and the post-test check response (triplicate average) were within 5% of their mean value, and the initial calibration linear regression data were used to quantify EO levels.

The results of the GC analyses were used to calculate EO levels in units of ppmvw. The data were combined with stack gas VFR and H<sub>2</sub>O data to calculate EO mass rates in units of pounds per hour (lb/hr) and concentrations in parts per million, dry volume basis (ppmvd). The catalytic oxidizer DRE was calculated on a mass basis.



pre and post each sampling period. Following sampling, the moisture gain in the impingers was measured gravimetrically and compared to the total sample volume (standard conditions) to determine the moisture content of the gas. The measured moisture content was compared to the saturation moisture content at stack temperature and pressure. The lower of the two moisture content values was reported.

# 3.3 U.S. EPA Reference Test Method 18 – Ethylene Oxide

Ethylene oxide concentrations were measured in accordance with EPA RM 18 using the direct interface sampling and analysis procedures detailed in the method. Samples were analyzed on-site with an HP Model 5890 Series II Gas Chromatograph equipped with dual RTX-1 columns to separate methane and EO, dual flame ionization detectors (FID) and Chemstation software.

Gas phase calibration standards were prepared by dilution of  $\pm$ 2% accuracy certified gas standards. Preparation of diluted standards were conducted using a gas-tight volumetric syringe and new Tedlar bags. Triplicate injections were conducted for each standard, and a calibration curve of peak area versus concentration was prepared. A least squares line (y=mx) was fit to the inlet and outlet data set.

Following the GC calibrations, a recovery study (line loss) was conducted using certified EO gas standards with approximate concentrations of 5000 ppm and 50 ppm of EO for the inlet and outlet sampling systems, respectively. A successful recovery study was demonstrated with the mean, triplicate GC response within 10% of the certified gas concentration.

Due to the presence of methane in the exhaust, prior to the test runs as well as during Run 2, a sample of exhaust gas was collected in a Tedlar bag. The contents of EO in the bag was quantified. Then the bag was spiked with a known concentration of EO to demonstrate adequate EO quantification and recovery. EO levels in the exhaust were below the reporting limit of 0.14 ppmvw.

EO levels were measured at the inlet and outlet simultaneously. A gas sample was transported directly to the GC gas sampling valves using a heated sample line. Samples were analyzed approximately once every 10-minutes. A "test run" consisted of five (5) consecutive injections. Three (3), test runs were conducted (for a total of 15 injections) at the inlet and outlet of the catalytic oxidizer.

After completing the 3 test runs, the mid-level calibration standards were re-analyzed at the gas sampling valve in triplicate. The average of the initial calibration response (triplicate average) and the post-test check response (triplicate average) were within 5% of their mean value, and the initial calibration linear regression data were used to quantify EO levels.

The results of the GC analyses were used to calculate EO levels in units of ppmvw. The data were combined with stack gas VFR and H<sub>2</sub>O data to calculate EO mass rates in units of pounds per hour (lb/hr) and concentrations in parts per million, dry volume basis (ppmvd). The catalytic oxidizer DRE will be calculated on a mass basis.

# Appendix A



Location	Becton-Dickinson Medical
Source	Catalytic Oxidizer - Outlet
Project No.	2019-0436
Run No.	1
Parameter(s)	EO, VFR

Meter Pressure (Pm), in. Hg

$$Pm = Pb + \frac{\Delta H}{13.6}$$

where,

$$\begin{array}{lll} Pb & 28.65 & = barometric pressure, in. \ Hg \\ \Delta H & 1.000 & = pressure \ differential \ of \ orifice, in \ H_2O \\ Pm & 28.72 & = in. \ Hg \end{array}$$

Absolute Stack Gas Pressure (Ps), in. Hg

$$Ps = Pb + \frac{Pg}{13.6}$$

where,

Standard Meter Volume (Vmstd), dscf

where, 
$$Vmstd = \frac{17.647 \times Vm \times Pm}{Tm}$$

$$\frac{Y}{Vm} = \frac{1.006}{37.437} = \text{meter correction factor}$$

$$\frac{Pm}{Tm} = \frac{28.72}{545.9} = \text{absolute meter pressure, in. Hg}$$

$$\frac{Vmstd}{Vmstd} = \frac{34.973}{34.973} = \text{dscf}$$

Standard Wet Volume (Vwstd), scf

Vmstd

$$Vwstd = 0.04707 \times Vlc$$

where,

$$\begin{array}{c|c} Vlc & 26.8 & = volume \ of \ H2O \ collected, \ ml \\ \hline Vwstd & 1.264 & = scf \end{array}$$

Moisture Fraction (BWSsat), dimensionless (theoretical at saturated conditions)

$$BWSsat = \frac{10}{P_S}$$
where,
$$Ts = \frac{139.3}{P_S} = \text{stack temperature, °F}$$

$$Ps = \frac{28.6}{D_S} = \text{absolute stack gas pressure, in. Hg}$$

$$= \frac{10}{P_S}$$

$$= \frac{10}{P_S}$$

$$= \frac{10}{P_S}$$

$$= \frac{139.3}{D_S} = \frac{139.3}{D_S}$$

$$= \frac{139.3}{D_S} = \frac{139.3}{D_S} = \frac{139.3}{D_S}$$

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Moisture Fraction (BWS), dimensionless

$$BWS = \frac{Vwstd}{(Vwstd + Vmstd)}$$

where,

Molecular Weight (WET) (Ms), lb/lb-mole

$$Ms = Md (1 - BWS) + 18 (BWS)$$

where,

$$\begin{array}{c|c} Md & 29.00 & = molecular weight (DRY), lb/lb mol \\ BWS & 0.035 & = moisture fraction, dimensionless \\ Ms & 28.62 & = lb/lb mol \\ \end{array}$$



Location	Becton-Dickinson Medical
Source	Catalytic Oxidizer - Outlet
Project No.	2019-0436
Run No.	1
Parameter(s)	EO, VFR

Average Velocity (Vs), ft/sec

$$Vs = 85.49 \times Cp \times (\Delta P^{-1/2}) avg \times \sqrt{\frac{Ts}{Ps \times Ms}}$$

where,

#### Average Stack Gas Flow at Stack Conditions (Qa), acfm

$$Qa = 60 \times Vs \times As$$

where,

Vs 
$$28.1$$
 = stack gas velocity, ft/sec = cross-sectional area of stack, ft<sup>2</sup> = acfm

#### Average Stack Gas Flow at Standard Conditions (Qs), dscfm

$$Qsd = 17.647 \times Qa \times (1 - BWS) \times \frac{Ps}{Ts}$$

where,

## Dry Gas Meter Calibration Check (Yqa), dimensionless

$$Y = \begin{pmatrix} \Theta & \sqrt{\frac{0.0319 \times Tm \times 29}{\Delta H @ \times \left(Pb + \frac{\Delta H \text{ avg.}}{13.6}\right) \times Md}} \sqrt{\Delta H} \text{ avg.} \\ Yqa = \frac{V}{V} \times \left(\frac{Pb + \frac{\Delta H \text{ avg.}}{13.6}}{V}\right) \times \frac{V}{V} \times \frac{V}{V} = \frac{V}{V} \times \frac{V$$

where,

Location: Becton-Dickinson Medical

Source: Catalytic Oxidizer - Outlet

**Project No.:** 2019-0436

# Carbon Monoxide Emission Rate (ER<sub>CO</sub>), lb/hr

$$ER_{EO} = \frac{C_{EO} \times MW \times Qs \times 60 \times 28.32}{24.04 \times 1.0E + 06 \times 454}$$

where,

$$\begin{array}{c|cccc} C_{EO} & 0.1 & = EO \ concentration, ppmvd \\ MW & 44.05 & = EO \ molecular \ weight, \ g/g-mole \\ Qs & 3,959 & = stack \ gas \ volumetric \ flow \ rate \ at \ standard \ conditions, \ dscfm \\ ER_{EO} & 0.0031 & = lb/hr \\ \end{array}$$

# Carbon Monoxide Reduction Efficiency (RE<sub>CO</sub>), %

$$RE_{EO} = \left(\frac{C_{EO-In} - C_{EO-Out}}{C_{EO-In}}\right) \times 100$$

where,

$$C_{EO-Out}$$
 0.0031 = EO Inlet Concentration (corrected), lb/hr  $C_{EO-In}$  23.56 = EO Outlet Concentration (corrected), lb/hr RE 99.99 = %

# Appendix B



# **Location Becton-Dickinson Medical**

# Source Catalytic Oxidizer

Project No. 2019-0436

Parameter(s): EO, VFR

Run Number		Run 1	Run 2	Run 3	Average
Date		7/12/19	7/12/19	7/12/19	
Start Time		9.:10	10:38	12:10	
Stop Time		10:10	11:38	13:10	
	Inlet Da	ata			
Volumetric Flow Rate, dscfm	(Qs)	4,022	4,008	3,772	3,934
Moisture Fraction	(BWS)	0.035	0.035	0.027	0.031
O2 Concentration, % dry	$(O_2)$	20.9	20.9	20.9	20.9
CO2 Concentration, % dry	$(CO_2)$	0.0	0.0	0.0	0.0
Ethylene Oxide Concentration, ppmvw	$C_{(EO)}$	824.22	1067.13	1329.86	1073.74
Ethylene Oxide Concentration, ppmvd	$C_{(EO)}$	854.00	1105.69	1366.33	1108.67
Ethylene Oxide Emission Rate, lb/hr	$ER_{(EO)}$	23.56	30.39	35.34	29.76
	Outlet I	<b>Data</b>			
Volumetric Flow Rate, dscfm	(Qs)	3,959	3,768	3,803	3,844
Moisture Fraction	(BWS)	0.035	0.035	0.027	0.016
O2 Concentration, % dry	$(O_2)$	20.9	20.9	20.9	20.9
CO2 Concentration, % dry	$(CO_2)$	0.0	0.0	0.0	0.0
Ethylene Oxide Concentration, ppmvw	$C_{(EO)}$	0.11	0.11	0.12	0.11
Ethylene Oxide Concentration, ppmvd	$C_{(EO)}$	0.11	0.11	0.12	0.12
Ethylene Oxide Emission Rate, lb/hr	$ER_{(EO)}$	0.0031	0.0029	0.0032	0.0031
	DRE Calcu	llations			
Ethylene Oxide Reduction Efficiency, %	ER(EO)	99.99	99.99	99.99	99.99



# **Method 1 Data**

**Location** Becton-Dickinson Medical

Source Catalytic Oxidizer - Inlet

Project No. 2019-0436

Date: 07/12/19

Stack Parameters

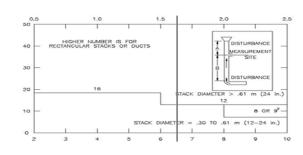
Duct Orientation: Horizontal
Duct Design: Circular
Distance from Far Wall to Outside of Port: 27.50 in
Nipple Length: 4.50 in

Depth of Duct: 23.00 in Cross Sectional Area of Duct: 2.89 ft No. of Test Ports: 2

Distance B Duct Diameters: 6.5 (must be > 2)

Minimum Number of Traverse Points: 12

Actual Number of Traverse Points: 16



#### CIRCULAR DUCT

					LOCATION (	F TRAVEF	RSE POINTS				
	Number of traverse points on a diameter										
	2	3	4	5	6	7	8	9	10	11	12
1	14.6		6.7		4.4		3.2		2.6		2.1
2	85.4		25.0		14.6		10.5		8.2		6.7
3			75.0		29.6		19.4		14.6		11.8
4			93.3		70.4		32.3		22.6		17.7
5					85.4		67.7		34.2		25.0
6					95.6		80.6		65.8		35.6
7							89.5		77.4		64.4
8							96.8		85.4		75.0
9									91.8		82.3
10									97.4		88.2
11											93.3
12											97.9

Traverse Point	from inside		Distance from outside of port
1	3.2	0.74	5.24
2	10.5	2.42	6.92
3	19.4	4.46	8.96
4	32.3	7.43	11.93
5	67.7	15.57	20.07
6	80.6	18.54	23.04
7	89.5	20.59	25.09
8	96.8	22.26	26.76
9			
10			
11			
12			

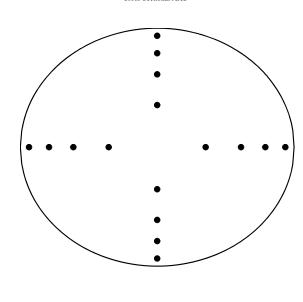
\*Percent of stack diameter from inside wall to traverse point.

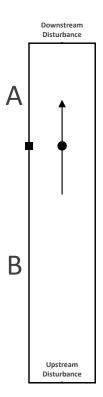
Stack Diagram

A = 5.42 ft.B = 12.5 ft.

B = 12.5 fDepth of Duct = 23 in.

Cross Sectional Area







# **Cyclonic Flow Check**

**Location Becton-Dickinson Medical** 

Source Catalytic Oxidizer - Inlet

Project No. 2019-0436

Date 7/12/19

Sample Point	Angle (ΔP=0)
1	3
2	2
3	3
4	3
5	2
6	1
7	5
8	4
9	6
10	3
11	2
12	2
13	7
14	1
15	2
16	5
Average	3.2



**Location Becton-Dickinson Medical** 

Source Catalytic Oxidizer - Inlet

Project No. <u>2019-0436</u>

Down No.		1	1 2			2	
Run No Date		1	7/12		<b>3</b> 7/12/19		
			7/12/19				
Status Start Time			VALID		VALID		
Start Time	7.55		11:08		12:35		
Stop Time			11:		12:40 Page 1		
Leak Check		iss	Pass		Pass		
Traverse Point	ΔP (in. WC)	Ts (°F)	Δ P (in. WC)	Ts (°F)	ΔP (in. WC)	Ts (°F)	
A1	0.17	90	0.23	91	0.21	97	
2	0.21	88	0.22	90	0.19	97	
3	0.23	88	0.21	89	0.18	92	
4	0.23	87	0.20	89	0.17	92	
5	0.22	87	0.22	88	0.19	91	
6	0.21	86	0.21	88	0.19	91	
7	0.22	85	0.20	88	0.20	92	
8	0.23	85	0.21	89	0.21	91	
B1	0.20	88	0.23	88	0.20	92	
2	0.23	88	0.22	88	0.19	92	
3	0.23	90	0.22	89	0.17	88	
4	0.26	91	0.19	89	0.20	90	
5	0.22	89	0.20	88	0.17	90	
6	0.23	89	0.23	91	0.17	92	
7	0.19	88	0.20	88	0.18	91	
8	0.16	87	0.18	91	0.18	91	
							Average
Square Root of $\Delta P$ , (in. WC) <sup>1/2</sup> $(\Delta P)^{1/2}$	0.4	63	0.4	59	0.4	433	0.451
Average ΔP, in. WC (ΔP)	0.3	22	0.2	.1	0.	19	0.20
Pitot Tube Coefficient (Cp)	0.8	314	0.8	14	0.0	314	0.814
Barometric Pressure, in. Hg (Pb)	28	.65	28.	65	28.65		28.65
Static Pressure, in. WC (Pg)	-7.	20	-7.	10	-7.10		-7.13
Stack Pressure, in. Hg (Ps)	28	.12	28.	13	28.13		28.13
Average Temperature, °F (Ts)	87	'.9	89	.0	91	1.8	89.6
Average Temperature, °R (Ts)	547.9		549.0		551.8		549.6
Measured Moisture Fraction (BWSmsd)							
Moisture Fraction @ Saturation (BWSsat)	0.0	)47	0.049		0.054		0.050
Moisture Fraction (BWS)	0.0	35	0.0	27	0.027		0.030
O2 Concentration, % (O2)	20	0.9	20.9		20.9		20.9
CO2 Concentration, % (CO2)	0	.0	0.	0	0	.0	0.0
Molecuar Weight, lb/lb-mole (dry) (Md)	29	.00	29.	00	29	.00	29.00
Molecuar Weight, lb/lb-mole (wet) (Ms)	28	.62	28.	70	28	.70	28.67
Velocity, ft/sec (Vs)	26	5.6	26	.3	24	4.9	25.9
VFR at stack conditions, acfm (Qa)	4,6	501	4,5	56	4,3	310	4,489
VFR at standard conditions, scfh (Qsw)	250	,070	247,	181	232	,609	243,287
VFR at standard conditions, scfm (Qsw)	4,1	68	4,1	20	3,877		4,055
/FR at standard conditions, dscfm (Qsd)	4,0	)22	4,0	08	3,7	772	3,934



# **Method 1 Data**

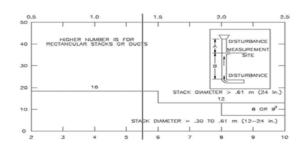
**Location** Becton-Dickinson Medical

Source Catalytic Oxidizer - Outlet
Project No. 2019-0436

Date: 07/12/19

# Stack Parameters

Duct Orientation:	Vertical	
Duct Design:	Circular	<u> </u>
Distance from Far Wall to Outside of Port:	27.50	in
Nipple Length:	4.00	in
Depth of Duct:	23.50	in
Cross Sectional Area of Duct:	3.01	ft <sup>2</sup>
No. of Test Ports:	2	<u> </u>
Distance A:	40.0	ft
Distance A Duct Diameters:	20.4	(must be > 0.5)
Distance B:	10.8	ft
Distance B Duct Diameters:	5.5	(must be > 2)
Minimum Number of Traverse Points:	16	<u> </u>
Actual Number of Traverse Points:	16	<u> </u>



# CIRCULAR DUCT

					LOCATION (	)F TRAVEF	RSE POINTS				
					Number of trav	erse points o	n a diameter				
	2	3	4	5	6	7	8	9	10	11	12
1	14.6		6.7		4.4		3.2		2.6		2.1
2	85.4		25.0		14.6		10.5		8.2		6.7
3			75.0		29.6		19.4		14.6		11.8
4			93.3		70.4		32.3		22.6		17.7
5					85.4		67.7		34.2		25.0
6					95.6		80.6		65.8		35.6
7							89.5		77.4		64.4
8							96.8		85.4		75.0
9									91.8		82.3
10									97.4		88.2
11											93.3
12											97.9

Traverse Point	% of Diameter	Distance from inside wall	Distance from outside of port
1	3.2	0.75	4.75
2	10.5	2.47	6.47
3	19.4	4.56	8.56
4	32.3	7.59	11.59
5	67.7	15.91	19.91
6	80.6	18.94	22.94
7	89.5	21.03	25.03
8	96.8	22.75	26.75
9			
10			
11			
12			

 $*Percent\ of\ stack\ diameter\ from\ inside\ wall\ to\ traverse\ point.$ 

Stack Diagram  $A = 40 \, \mathrm{ft}.$   $B = 10.8 \, \mathrm{ft}.$ Depth of Duct = 23.5 in. Cross Sectional Area





# **Cyclonic Flow Check**

**Location Becton-Dickinson Medical** 

Source Catalytic Oxidizer - Outlet Project No. 2019-0436

Date 7/12/19

Sample Point	Angle (ΔP=0)
1	2
2	4
3	1
4	3
5	2
6	5
7	7
8	6
9	4
10	3
11	3
12	4
13	1
14	2
15	4
16	2
Average	3.3



**Location Becton-Dickinson Medical** 

Source Catalytic Oxidizer - Outlet

Project No. <u>2019-0436</u>

	Run No.	1		2			3	
	Date	7/12		7/12			2/19	
	Status	VAI		VAI			LID	
	Start Time	9:2		10:.			:48	
	Stop Time	9:2 P		11:			:56	
	Leak Check	Pa		Pas			ass	
Traverse Point		Δ P (in. WC)	Ts (°F)	ΔP (in. WC)	Ts (°F)	ΔP (in. WC)	Ts (°F)	
A1		0.15	147	0.15	136	0.14	128	
2		0.18	144	0.16	135	0.18	129	
3		0.22	128	0.20	136	0.20	127	
4		0.22	126	0.20	141	0.20	123	
5		0.21	134	0.21	141	0.21	121	
6		0.22	147	0.23	135	0.19	122	
7		0.23	152	0.21	138	0.22	122	
8		0.23	152	0.22	130	0.21	122	
B1		0.17	134	0.16	145	0.15	118	
2		0.22	132	0.22	136	0.17	116	
3		0.25	133	0.23	140	0.23	120	
4		0.28	135	0.18	142	0.22	121	
5		0.27	140	0.21	137	0.24	120	
6		0.26	141	0.21	131	0.20	120	
7		0.25	141	0.21	136	0.20	120	
8		0.23	142	0.19	136	0.21	122	
	1			1		1		Average
Square Root of ΔP, (in. WC) <sup>1/2</sup> (A	$(\Delta P)^{1/2}$	0.4	72	0.44	46	0.4	144	0.454
Average ΔP, in. WC	(ΔΡ)	0.2	22	0.2	20	0.	20	0.21
Pitot Tube Coefficient	(Cp)	0.8	14	0.8	14	0.8	314	0.814
Barometric Pressure, in. Hg	(Pb)	28.	65	28.0	65	28	.65	28.65
Static Pressure, in. WC	(Pg)	-0	21	-0.1	17	-0	.18	-0.19
Stack Pressure, in. Hg	(Ps)	28.	63	28.0	64	28	.64	28.64
Average Temperature, °F	(Ts)	139	9.3	137	7.2	12	1.9	132.8
Average Temperature, °R	(Ts)	599	9.3	597	1.2	58	1.9	592.8
Measured Moisture Fraction (BV	VSmsd)		_		-	-	<b></b>	
Moisture Fraction @ Saturation (BV	WSsat)	0.2	02	0.19	91	0.1	127	0.173
Moisture Fraction (I	BWS)	0.0	35	0.02	27	0.0	)27	0.030
O2 Concentration, %	(O2)	20	.9	20.	.9	20	).9	20.9
CO2 Concentration, %	CO2)	0.	0	0.0	0	0	.0	0.0
Molecuar Weight, lb/lb-mole (dry) (	(Md)	29.	00	29.0	00	29	.00	29.00
Molecuar Weight, lb/lb-mole (wet)	(Ms)	28.	62	28.	70	28	.70	28.67
Velocity, ft/sec	(Vs)	28	.1	26.	.4	26	5.0	26.8
VFR at stack conditions, acfm	(Qa)	4,8	65	4,5′	77	4,5	501	4,648
VFR at standard conditions, scfh (	Qsw)	246,	148	232,	383	234	,535	237,689
VFR at standard conditions, scfm (	Qsw)	4,1	02	3,8′	73	3,9	909	3,961
/FR at standard conditions, dscfm (	Qsd)	3,9	59	3,70	68	3,8	303	3,844



Location Becton-Dickinson Medical Source Catalytic Oxidizer - Outle Project No. 2019-0436 Parameter(s): EO, VFR Console Type Meter Box

Run No.				1					2					3		
Date				7/12/19					7/12/19					7/12/19		
Status				VALID					VALID					VALID		
Start Time				9.:10					10:38					12:10		
End Time				10:10					11:38					13:10		
Run Time, min	(θ)			60					60					60		
Meter ID	(0)			M5-25					M5-25					M5-25		
Meter Correction Factor	(Y)			1.006					1.006					1.006		
Orifice Calibration Value	(AH @)			1.560					1.560					1.560		
Max Vacuum, in. Hg	(311 (6)			4					3					4		
Post Leak Check, ft3/min (at max vac.)				0.000					0.000					0.000		
Meter Volume, ft3				0.000					0.000					0.000		
0				113.879					151.512					190.261		
5				116.900					154.700					193.400		
10				120.000					157.900					196.600		
15				123.100					161.100					199.800		
20				126.200					164.200					203.100		
25				129.700					167.300					206.200		
30				132.400					170.500					209.400		
35			132.400 135.700						173.600					212.600		
40				139.000					176.800					215.900		
45				142.100					179.900					218.900		
50				145.300					183.100					222.100		
55				148.300					186.200					225.400		
60				151.316					189.379					228.670		
Total Meter Volume, ft3	(Vm)			37.437					37.867					38.409		
Temperature, °F	( )	Meter	Probe	Filter	Vacuum	Imp. Exit	Meter	Probe	Filter	Vacuum	Imp. Exit	Meter	Probe	Filter	Vacuum	Imp. Exit
0		78	252	252	4	58	91	252	252	3	58	95	252	252	4	58
5		78	252	252	4	58	91	252	252	3	58	95	252	252	4	58
10		80	252	252	4	57	92	252	252	3	59	96	253	253	4	57
15		81	253	253	4	55	92	253	253	3	60	97	253	253	4	55
20		82	253	253	4	54	93	253	253	3	60	97	253	253	4	55
25		85	253	253	4	54	95	252	252	3	58	97	252	252	4	55
30		87	252	252	4	55	95	252	252	3	58	98	252	252	4	56
35		88	252	252	4	55	98	253	253	3	58	101	252	252	4	58
40		90	252	252	4	56	99	253	253	3	57	102	252	252	4	58
45		91	252	252	4	56	100	253	253	3	56	103	253	253	4	59
50		93	253	253	4	57	101	253	253	3	56	104	253	253	4	60
55		92	252	252	4	57	102	252	252	3	55	104	253	253	4	61
60		95	252	252	4	58	102	252	252	3	55	105	253	253	4	61
Average Temperature, °F	(Tm)	86	252	252			96	252	252			100	253	253		
Average Temperature, °R	(Tm)	546	712	712			556	712	712			559	712	712		
Minimum Temperature, °F		78	252	252			91	252	252			95	252	252		
Maximum Temperature, °F		95	253	253		58	102	253	253		60	105	253	253		61
Barometeric Pressure, in. Hg	(Pb)			28.65					28.65					28.65		
Meter Orifice Pressure , in. WC	(AH)			1.000					1.000					1.000		
Meter Pressure, in. Hg	(Pm)			28.72					28.72					28.72		
Standard Meter Volume, ft3	(Vmstd)			34.973					34.733					35.022		
Analysis Type				Gravimetri					Gravimetrio					Gravimetri		
Impinger 1, Pre/Post Test, mL		H		875.0	919.3	44.3		20	919.3	925.4	6.1	H2		925.4	932.3	6.9
Impinger 2, Pre/Post Test, mL		H		853.8	825.1	-28.7		20	825.1	833.6	8.5	H2		827.6	831.8	4.2
Impinger 3, Pre/Post Test, mL		Em		638.8	642.1	3.3		npty	640.6	642.1	1.5	Em		641.1	643.6	2.5
Impinger 4, Pre/Post Test, g	071.)	Sil	ıca	907.9	915.8	7.9	Sıl	lica	915.8	919.9	4.1	Sil	ıca	919.9	927.0	7.1
Volume Water Collected, mL Standard Water Volume, ft	(Vlc)			26.8					20.2					20.7 0.976		
Standard Water Volume, It Moisture Fraction Measured	(Vwstd) (BWS)			1.264					0.952							
				0.035					0.027					0.027		
Static Pressure, in. WC	(Pg)			-0.21					-0.17					-0.18		
Stack Pressure, in. Hg	(Ps)			28.63					28.64					28.64		
Stack Temperature, °F	(Ts)			131 29.00					125 29.00					138 29.00		
Gas Molecular Weight, lb/lb-mole (dry) DGM Calibration Check Value	(Md) (Yqa)			0.7					0.9					29.00		
DGM Candration Check value	(Yqa)			0./					0.9					2.0		

# Appendix C

			Initial	Three-Poi	nt Calibration					
			(Inlet) High	n Level Ca	libration Stand	lard				
Cpd	Conc.	li li	nj. 1	I	nj. 2	I	nj. 3		Average	
ID	(ppm)	RT	AC	RT	AC	RT	AC	RT	AC	OK?
Ethylene Oxide	5179.00	3.906	9631715.0	3.912	9635232.0	3.912	9640443.0	3.910	9635797	Υ
			Mid-Le	vel Calibra	ation Standard					
Cpd	Conc.	li li	nj. 1	I	nj. 2	I	nj. 3		Average	
ID	(ppm)	RT	AC	RT	AC	RT	AC	RT	AC	OK?
Ethylene Oxide	2589.50	3.890	4730595.5	3.895	4764450.5	3.898	4749841.0	3.894	4748296	Υ
			Low-Le	evel Calibra	ation Standard	i				
C=4	Conc.	lnj. 1	Sig.20015	lnj. 2	Sig.20016	Inj. 3	Sig.20017		Average	
Cpd								DT	• •	
iD	(ppm)	RT	AC	RT	AC	RT	AC	RT	AC	OK?

			Initial	Three-Poir	nt Calibration					
			(Outlet) Lo	w Level Ca	libration Stan	dard				
Cpd	Conc.	In	j. 1	li li	nj. 2	li	nj. 3		Average	
ID	(ppm)	RT	AC	RT	AC	RT	AC	RT	AC	OK?
Ethylene Oxide	50.02	4.222	172921.2	4.24	172524.5	4.24	172641.4	4.234	172696	Υ
			Mid-Le	vel Calibra	tion Standard	l				
Cpd	Conc.	In	j. 1	li li	nj. 2	li	nj. 3		Average	
ID	(ppm)	RT	AC	RT	AC	RT	AC	RT	AC	OK?
Ethylene Oxide	25.01	4.152	90423.1	4.172	91117.8	4.191	88411.7	4.172	89984	Υ
			Low-Le	evel Calibra	tion Standard	1				
Cpd	Conc.	In	j. 1		nj. 2		nj. 3		Average	
ID	(ppm)	RT	AC	RT	AC	RT	AC	RT	AC	OK?
Ethylene Oxide	12.51	4.200	48065.7	4.200	48189.4	4.212	47008.1	4.204	47754	Υ

		Lir	near Regression	on Calculation	ns			
	Ethyle	ene Oxide - Inlet			Ethyl	ene Oxide	- Outlet	
Certified ppm	Average AC	Linear Regression Statistics	ppm from curve	Certified ppm	Average AC	Linear F	Regression tistics	ppm from curve
5179.00 2589.50 1294.75	9635797 4748296 2345909	<b>R</b> <sup>2</sup> <b>M</b> 1.0000 0.0005396	5199.49 2562.19 1265.86	50.02 25.01 12.51	172696 89984 47754	<b>R</b> <sup>2</sup> 1.0000	<b>M</b> 0.0002857	49.34 25.71 13.64
50 40 mdd - 30 20 20 20 20 20 20 20 20 20 20 20 20 20	000.00 000.00 000.00 000.00 000.00 0.00	2000000 4000	000 60000 Area Counts Oxide - Inlet	000 80000 ——————————————————————————————			60.00 50.00 40.00 30.00 20.00 10.00 120000000	Outlet -ppm

				Qual	ity Assurance	Inlet							
	Inlet Line Loss Check (High-level calibration gas to the sample probe)												
Cpd	Conc.	lnj. 1	Sig. 10059	lnj. 2	Sig. 10060	Inj. 3	Sig.10061	Average			Triplicate	Recovery	
ID	(ppm)	RT	AC	RT	AC	RT	AC	RT	AC	ppm	OK?	OK?	
Ethylene Oxide	5179.00	3.912	9639243	3.912	9632581	3.914	9638738	3.913	9636854	5200.06	Y	Y	

	Inlet Post Test Calibration Check (mid-level calibration gas to the gas sampling valve)												
Cpd	Conc.	lnj. 1				Inj. 3 Average					Triplicate	Pre/Post	
ID	(ppm)	RT	AC	RT	AC	RT	AC	RT	AC	ppm	OK?	OK?	
Ethylene Oxide	2589.50	3.877	4717307.5	3.871	4693612.5	3.874	4671855.5	3.874	4694259	2533.03	Y	Y	

Quality Assurance Outlet													
	Outlet Line Loss Check (High-level calibration gas to the sample probe)												
Cpd	Conc.	lnj. 1	Sig.20059	lnj. 2	Sig. 20060	Inj. 3	Sig.20061	Average			Triplicate	Recovery	
ID	(ppm)	RT	AC	RT	AC	RT	AC	RT	AC	ppm	OK?	OK?	
Ethylene Oxide	50.02	4.238	169723.5	4.242	169468.1	4.25	172564	4.243	170585	48.74	Υ	Υ	

Outlet Post Test Calibration Check (mid-level calibration gas to the gas sampling valve)													
Cpd	Conc.	lnj. 1	Sig.10043	lnj. 2	Sig.10044	Inj. 3	Sig.10045	Average			Triplicate	Pre/Post	
ID	(ppm)	RT	AC	RT	AC	RT	AC	RT	AC	ppm	OK?	OK?	
Ethylene Oxide	25.01	4.005	96791.2	3.986	96755.6	3.99	96361.3	3.994	96636	27.61	Y	Υ	

						Analysis (In	let)						
Cpd	1	lnj. 1	In	j. 2		Run 1 i. 3	le le	j. 4	le le	ij. 5		Avorago	
		•									DT	Average	
ID	RT	AC	RT	AC	RT	AC	RT	AC	RT	AC	RT	AC	ppm
Ethylene Oxide	3.92	373377.1	3.917	1987208	3.922	2062162	3.92	2066465	3.926	1148072	3.921	1527457	824.22
						Run 2							
Cpd		lnj. 1	In	j. 2	In	j. 3	In	j. 4	In	ij. 5			
ID	RT	AC	RT	AC	RT	AC	RT	AC	RT	AC	RT	AC	ppm
Ethylene Oxide	3.92	2033142.9	3.918	1739798	3.917	2018769	3.916	2010283	3.913	2086107	3.917	1977620	1067.13
						Run 3							
Cpd		lnj. 1	In	j. 2	ln,	j. 3	In	j. 4	In	ij. 5		Average	
ID	RT	AC	RT	AC	RT	AC	RT	AC	RT	AC	RT	AC	ppm

					Sample A	nalvsis (Oı	ıtlet)						
						Run 1	atietj						
Cpd	Inj	j. 1	lnj	i. 2	lnj	. 3	lnj	. 4	lnj	. 5		Average	
ID	RT	AC	RT	AC	RT	AC	RT	AC	RT	AC	RT	AC	ppm
Ethylene Oxide	3.544	402.1	3.56	395.1	3.534	412.4	3.535	395.4	3.544	380.3	3.543	397	0.11
Cnd	Ini	i 1	Ini	. 2		Run 2	Ini	4	Ini	5	1	Avorago	
0	1 1-1		1 1				1		11	_	1	A	
Cpd ID		j. 1 AC		j. 2 AC	lnj	. 3		. 4 AC	lnj RT		RT	Average	ppm
İD	RT	j. 1 AC 387.8	RT 3.501	j. 2 AC 389.9			RT 3,499	. <b>4</b> AC 362.9	Inj RT 3.497	. <b>5</b> AC 371.7	RT 3.509	Average AC 377	<b>ppm</b> 0.11
İD		AC	RT	AC	Inj RT	. 3 AC	RT	AC	RT	AC		AC	
İD	RT	AC	RT	AC	Inj RT 3.506	. 3 AC	RT	AC	RT	AC		AC	
İD	RT 3.540	AC	<b>RT</b> 3.501	AC	Inj RT 3.506	AC 372.5	<b>RT</b> 3.499	AC	RT	<b>AC</b> 371.7		AC	
ID Ethylene Oxide	RT 3.540	AC 387.8	<b>RT</b> 3.501	AC 389.9	Inj RT 3.506	AC 372.5	<b>RT</b> 3.499	<b>AC</b> 362.9	<b>RT</b> 3.497	<b>AC</b> 371.7		AC 377	



S-type Pitot ID:

P-674

Date: 13-Jan-11

Standard Pitot ID:

001

Personnel:

**WB** 

Cp(std):

0.99

Cp(actual):

0.814

Part Number:

PPST12-Y-036

P(bar):

29.80

Test Velocity (fps):

**50** 

T(°F):

33

ΔP <sub>std</sub> (in. H <sub>2</sub> 0)	$\Delta P_s$ (in. $H_2 0$ )	Cp(s)	Deviation*
0.599	0.898	0.809	-0.003
0.601	0.894	0.812	-0.001
0.603	0.889	0.815	0.003
0.601	0.891	0.813	0.001
	AVERAGE	0.812	0.002
<b>L</b>		Std deviation	0.003

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ΔP <sub>std</sub> (in. H <sub>2</sub> 0)	ΔP <sub>s</sub> (in. H <sub>2</sub> 0)	Cp(s)	Deviation*
0.595	0.871	0.818	0.002
0.597	0.873	0.819	0.002
0.593	0.876	0.814	-0.002
0.594	0.879	0.814	-0.002
	AVERAGE	0.816	0.002
_		Std deviation	0.003

$$Cp(s) = Cp(std)\sqrt{\frac{\Delta P(std)}{\Delta P(s)}}$$

$$Cp(A) - Cp(B) = 0.004$$
 {must be <0.010}

\*Deviation =  $\{Cp(s) - AVGCp(s)\}\ \{must be < 0.010\}$ 

Standard deviation of the deviations must be less than 0.02 for both sides.

Pitot tube S/N P-674 was calibrated in accordance with the CFR 40, Part 60 Appendix A, Method 2, Section 10.

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#### METHOD 5 DRY GAS METER CALIBRATION USING CRITICAL ORIFICES

- 1) Select three critical orifices to calibrate the dry gas meter which bracket the expected operating range.
- 2) Record barometric pressure before and after calibration procedure.
- 3) Run at tested vacuum (from Orifice Calibration Report), for a period of time necessary to achieve a minimum volume of 10 cubic feet Vcr (STD). K' factors of ~. 8025 = 13 minutes, .5011 = 20 minu
- 4) Record data and information in the GREEN cells, YELLOW cells are calculated.

INITIAL FINAL AVG (P<sub>bar</sub>) BAROMETRIC PRESSURE (mbar): 833 834 833.5 INITIAL FINAL AVG (P<sub>bar</sub>) BAROMETRIC PRESSURE (in Hg): 24.59849 24.6280 24.6133 TECHNICIAN/OPERATOR: Phil Brock

DATE:	5/8/2019
METER PART #:	NA

DGM SERIAL NUMBER:	18654624
CRITICAL ORIFICE MFG:	Apex
METHOD 5 BOX ID:	M5-25

		K'	TESTED	_					TEN	MPERATU	RES °F			ELAPSED					
		FACTOR	VACUUM		DGN	/ READINGS (	FT <sup>3</sup> )	AMBIENT	DGM II	NLET	DGM O	UTLET	DGM	TIME (MIN)	DGM ΔH	(1)	(2)	(3)	
ORIFICE #	RUN#	(AVG)	(in Hg)		INITIAL	FINAL	NET (V <sub>m</sub> )		INITIAL	FINAL	INITIAL	FINAL	AVG	θ	(in H <sub>2</sub> O)	V <sub>m</sub> (STD)	V <sub>cr</sub> (STD)	Υ	$\Delta H_{@}$
-	1			Г			Ī		1				Ì						
	1	0.3433	19.5		223.0	233.252	10.252	72	77	74	77	75	75.75	23.0	0.44	8.3239	8.4283	1.013	1.48
48	2	0.3433	19.5	L	245.002	255.271	10.269	71	74	75	75	77	75.25	23.0	0.44	8.3455	8.4363	<u>1.011</u>	1.48
	3	0.3433	19.5		255.271	265.515	10.244	71	75	73	77	74	74.75	23.0	0.44	8.3330	8.4363	1.012	1.48
	1			г		1	Ī		1	1			Ì				AVG =	1.012	
	1	0.5849	17.0	Ļ	265.515	276.159	10.644	71	76	78	75	78	76.75	14.0	1.35	8.6497	8.7490	<u>1.011</u>	1.58
63	2	0.5849	17.0	L	276.159	286.875	10.716	71	78	76	78	77	77.25	14.0	1.35	8.7001	8.7490	1.006	1.58
	3	0.5849	17.0		286.875	297.556	10.681	71	76	74	77	75	75.5	14.0	1.35	8.70	8.7490	1.006	1.58
	1			г		1	Ī		ı	1			1				AVG =	1.008	
	1	0.8025	15.0	L	297.556	308.057	10.501	71	74	77	75	75	75.25	10.0	2.60	8.5892	8.5742	0.998	1.63
73	2	0.8025	15.0		308.057	318.617	10.560	71	77	82	75	79	78.25	10.0	2.60	8.5893	8.5742	0.998	1.62
	3	0.8025	15.0		318.617	329.223	10.606	71	82	79	79	80	80	10.0	2.60	8.5987	8.5742	0.997	1.61
	= '						•										AVG =	0.998	

#### USING THE CRITICAL ORIFICES AS CALIBRATION STANDARDS:

The following equations are used to calculate the standard volumes of air passed through the DGM, V<sub>m</sub> (std), and the critical orifice, V<sub>cr</sub> (std), and the DGM calibration factor, Y. These equations are automatically calculated in the spreadsheet above.

1.006 AVERAGE DRY GAS METER CALIBRATION FACTOR, Y =

AVERAGE ΔH<sub>@</sub> = 1.56

(1) 
$$Vm_{(std)} = K_1 * Vm * \frac{Pbar + (\Delta H / 13.6)}{Tm}$$

= Net volume of gas sample passed through DGM, corrected to standard conditions K<sub>1</sub> = 17.64 °R/in. Hg (English), 0.3858 °K/mm Hg (Metric)

T<sub>m</sub> = Absolute DGM avg. temperature (°R - English, °K - Metric)

 $\Delta H_{@} = \left(\frac{0.75 \, \theta}{V_{cr}(std)}\right)^2 \, \Delta H \left(\frac{V_{m}(std)}{V_{m}}\right)$ 

(2) 
$$Vcr_{(ztd)} = K'* \frac{Pbar * \Theta}{\sqrt{Tamb}}$$

= Volume of gas sample passed through the critical orifice, corrected to standard conditions T<sub>amb</sub> = Absolute ambient temperature (°R - English, °K - Metric)

K' = Average K' factor from Critical Orifice Calibration

 $Vm_{(std)}$ 

= DGM calibration factor

Pyrometer Calibration Data

Calibration Temp. Reading (F)	Pyrometer Reading (F)	ABS (Relative Difference) % R
0	2	0.4
50	50	0.0
100	99	0.2
150	150	0.0
250	252	0.3
500	499	0.1
800	802	0.2
Max Absolute Diffe	rence %	0.4

Omega Temp Calibrator ID 1 Omega Temp Calibrator S/N. T-197197 Calibration Date......7/27/2017 Recert Date......7/27/2018



# **CERTIFICATE OF ANALYSIS**

# **Grade of Product: CERTIFIED STANDARD-SPEC**

Customer:

ALLIANCE SOURCE TESTING

Part Number:

X02NI99C15A5263 ALM-014712

Cylinder Number:

124 - La Porte Mix - TX Laboratory:

Analysis Date: Lot Number:

Jul 01, 2019 126-401527371-1

Expiration Date: Jul 01, 2021

# Airgas USA, LLC

616 Miller Cut Off Rd. LaPorte, TX 77571 281-842-6900 Airgas.com

Reference Number: Cylinder Volume:

Cylinder Pressure: Valve Outlet:

126-401527371-1 144.4 CF

2015 PSIG 350SS

Product composition verified by direct comparison to calibration standards traceable to N.I.S.T. weights and/or N.I.S.T. Gas Mixture reference materials.

# ANALYTICAL RESULTS

Component

Req Conc

**Actual Concentration** 

**Analytical** Uncertainty

(Mole %)

ETHYLENE OXIDE

50.00 PPM

50.02 PPM

+/- 2%

**NITROGEN** 

Balance

Notes:

\*\*RECERTIFICATION\*\* ALLIANCE SOURCE TESTING







# **CERTIFICATE OF ANALYSIS**

# **Grade of Product: CERTIFIED STANDARD-SPEC**

Customer:

ALLIANCE SOURCE TESTING

Part Number:

X02NI99C15A0631

Cylinder Number:

ALM013685

Laboratory: Analysis Date: Lot Number: 124 - La Porte Mix - TX Jul 03, 2019

126-401542179-1

Expiration Date: Jul 03, 2020

Airgas USA, LLC

616 Miller Cut Off Rd. LaPorte, TX 77571 281-842-6900

Airgas.com

Reference Number: Cylinder Volume:

Cylinder Pressure:

Valve Outlet:

126-401542179-1

144.9 CF

2015 PSIG

350

Product composition verified by direct comparison to calibration standards traceable to N.I.S.T. weights and/or N.I.S.T. Gas Mixture reference materials.

# ANALYTICAL RESULTS

Component

**Req Conc** 

**Actual Concentration** 

(Mole %)

Analytical

Uncertainty

ETHYLENE OXIDE

5210 PPM

Balance

5179 PPM

+/- 2%

Notes:

**NITROGEN** 

\*\*RECERTIFICATION\*\*
ALLIANCE SOURCE TESTING



Approved for Release

# Appendix D

nte: 12 Jul 1	9	Recorded By								
Time	% LEL	Recorded By: Darin Meyer,								
	30.630	% LEL 30.633	Inlet Bed Temp *C	Outlet Bed Ter						
13:06	5.1	4.7	(Control) 25.610	25.611						
13:10	5.1	4.5	161	19.5						
13.20	5.2	5.6	160	196						
13:3e	5.4	5 1	142	196						
13:40	3,8	3,5	141	194						
13.50	4.1	4.6	162	902						
14.00	3,2	3,0	165	201						
14:10	4.7	4.4	163	179						
14:20	5,6	5,2	164	203						
14:30	3.(	2.8	164	199						
14:40	н. 2	3.9	164	202						
14:50	3.1	2.8	166	203						
15:00	5.0	4.7	164	201						
				12						
				1 3 8						
J. 15 (30)										

# **Lesni Stack Test Data**

Date: 12 Jul 19

Recorded By: Darin Meyer

	Time	% LEL 30.630	% LEL 30.633	Inlet Bed Temp °C (Control) 25.610	Outlet Bed Temp °C 25.611
-	8:50 AM	0.2	0.0	161	161
	9:00 Ay	0.3	0.0	161	161
CHIT -	9:10 AM	0.3	0.0	161	141
-	9:20 AM	0.9	0.5	159	161
	9:30 AM	1.0	0.5	159	160
-	9:40 Ag	3.0	2,7	160	161
-	9:50 AM	3.0	2.5	159	164
	10:00 AM	3.5	3.1	161	170
	10:10 Am	3,4	2.9	159	177
In 2	10:00 AM	3.4	3.0	140	182
	10:30 AM	3.4	2.7	161	184
	10:4049	3,2	3,0	161	185
	10:50 AM	2.6	2.2	159	182
	11:00 AM	3.1	2. 3	141	184
	11:10AM	3 (	2.7	159	185
	11:20 AM	3.1	2.8	160	185
22	11:30 AM	2.9	2.6	159	186
	11:40	3.0	2.6	160	185
	11:50	3.4	3.1	161	186
	12:00	1,1	1.0	160	187
	12:10	3.8	3.5	160	187
	17:30	3.1	2.5	160	186
	12.30	3.7	3.5	159	184
	12:40	3.1	3.5	159	188
	12:50	4-1	4.0	(59	189

**Last Page of Report**